

Industry Day Theme # Emerging Nano and Advanced Materials

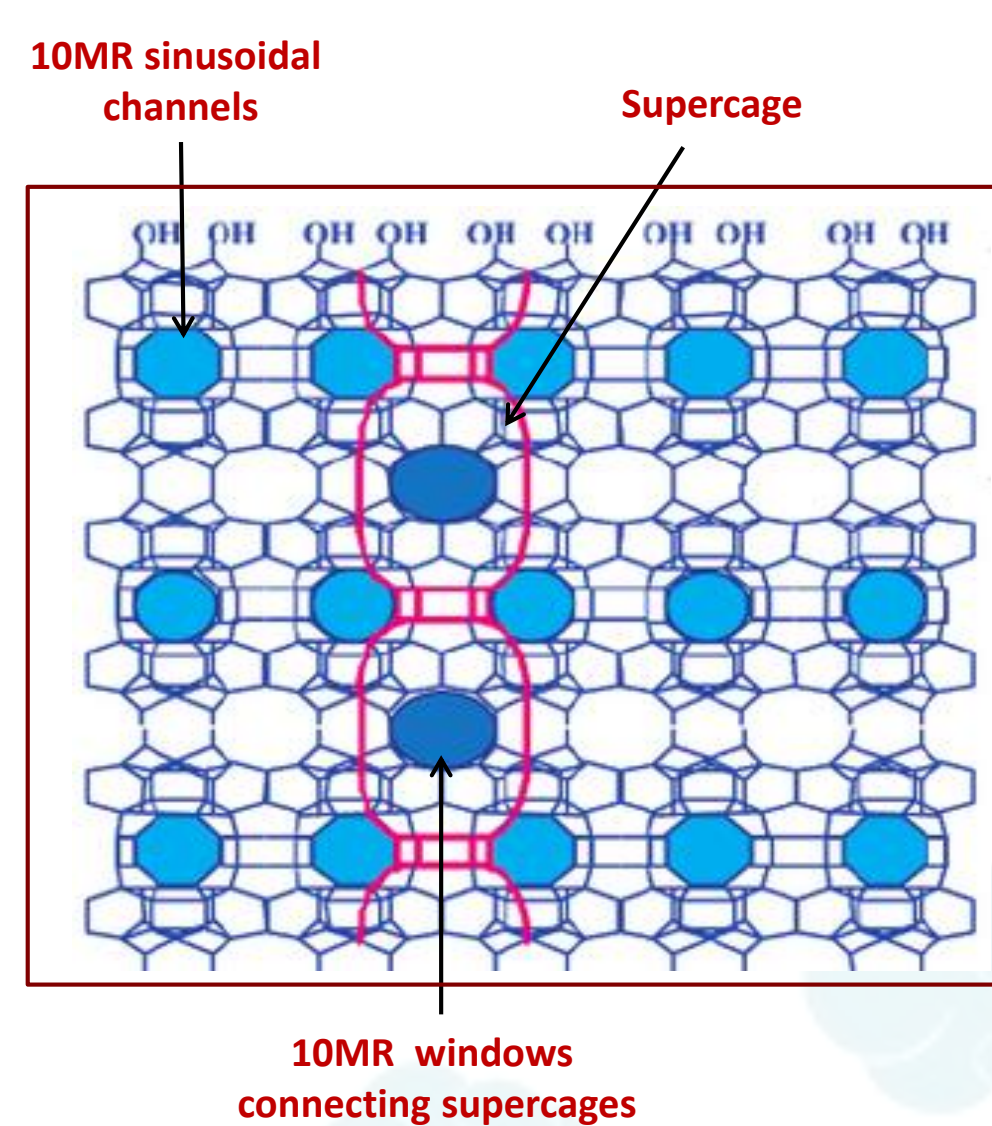
HMCM-22 zeolite with different Si/Al₂ ratios: Synthesis and Catalytic Properties in Methane Dehydroaromatization

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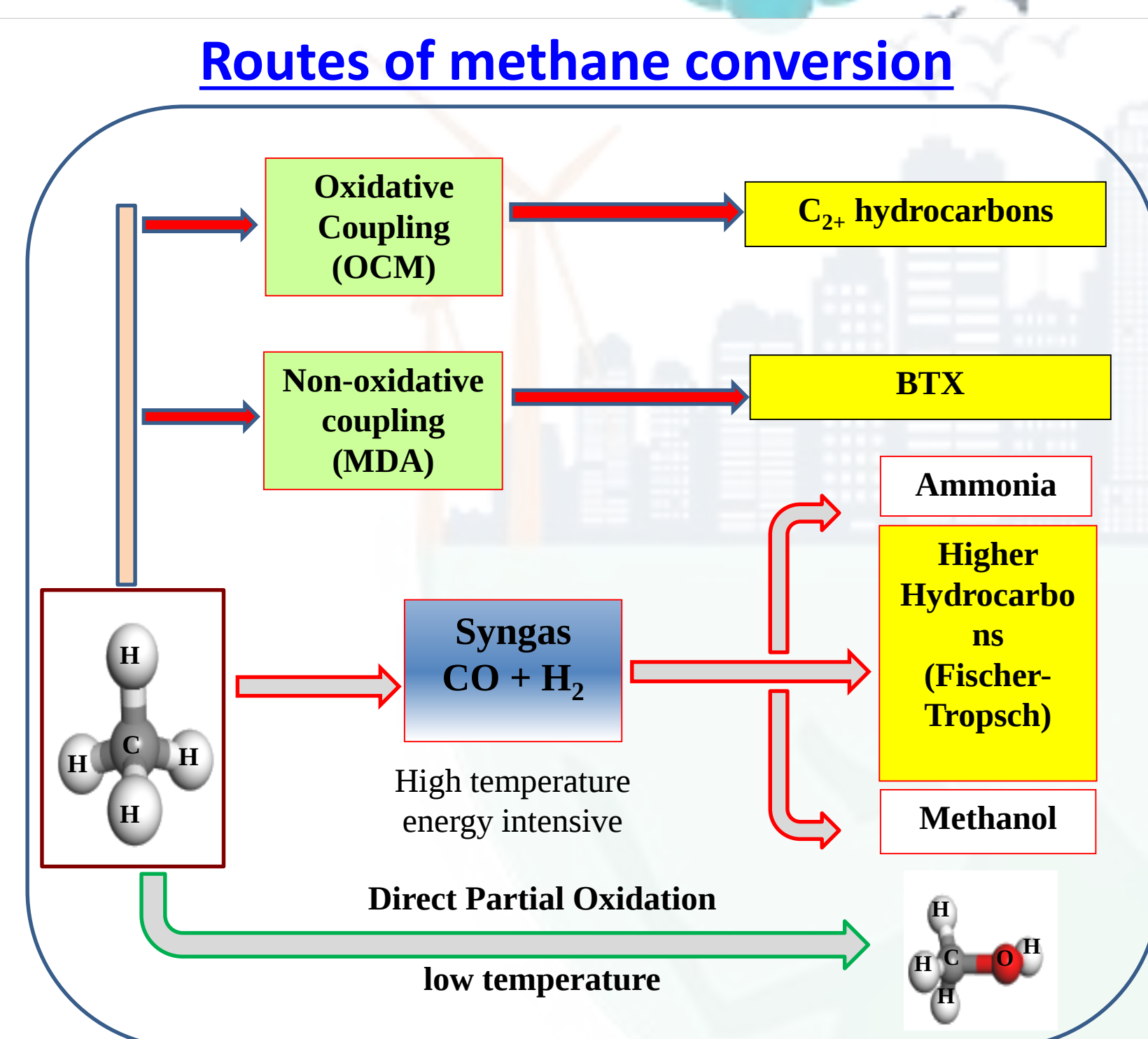
Abstract

- HMCM-22 zeolite is a potential catalyst for petrochemical industries
- Key catalyst for different aromatic alkylation and isomerization reactions
- Highly effective in Methane dehydroaromatization (MDA) process than the conventional ZSM-5 catalyst with molybdenum (Mo)

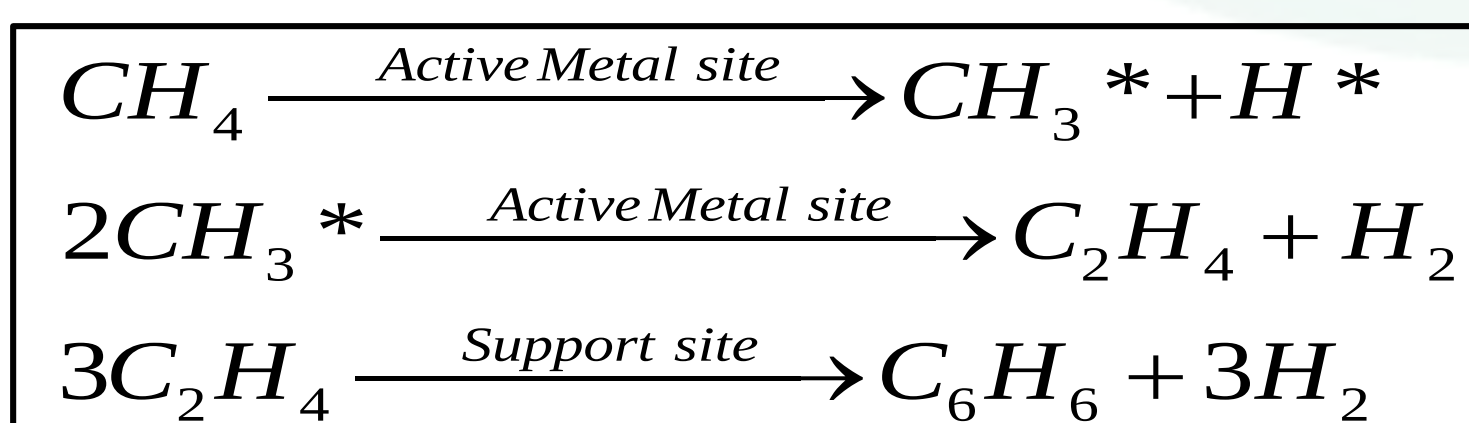


Introduction

- Natural gas availability at remote locations imparts high transportation cost
- Current commercial processes via indirect path require economy of scale
- Direct conversion of methane into higher hydrocarbons is an efficient process for natural gas upgradation
- Zeolite supported molybdenum catalysts are among the most promising catalysts for this process.



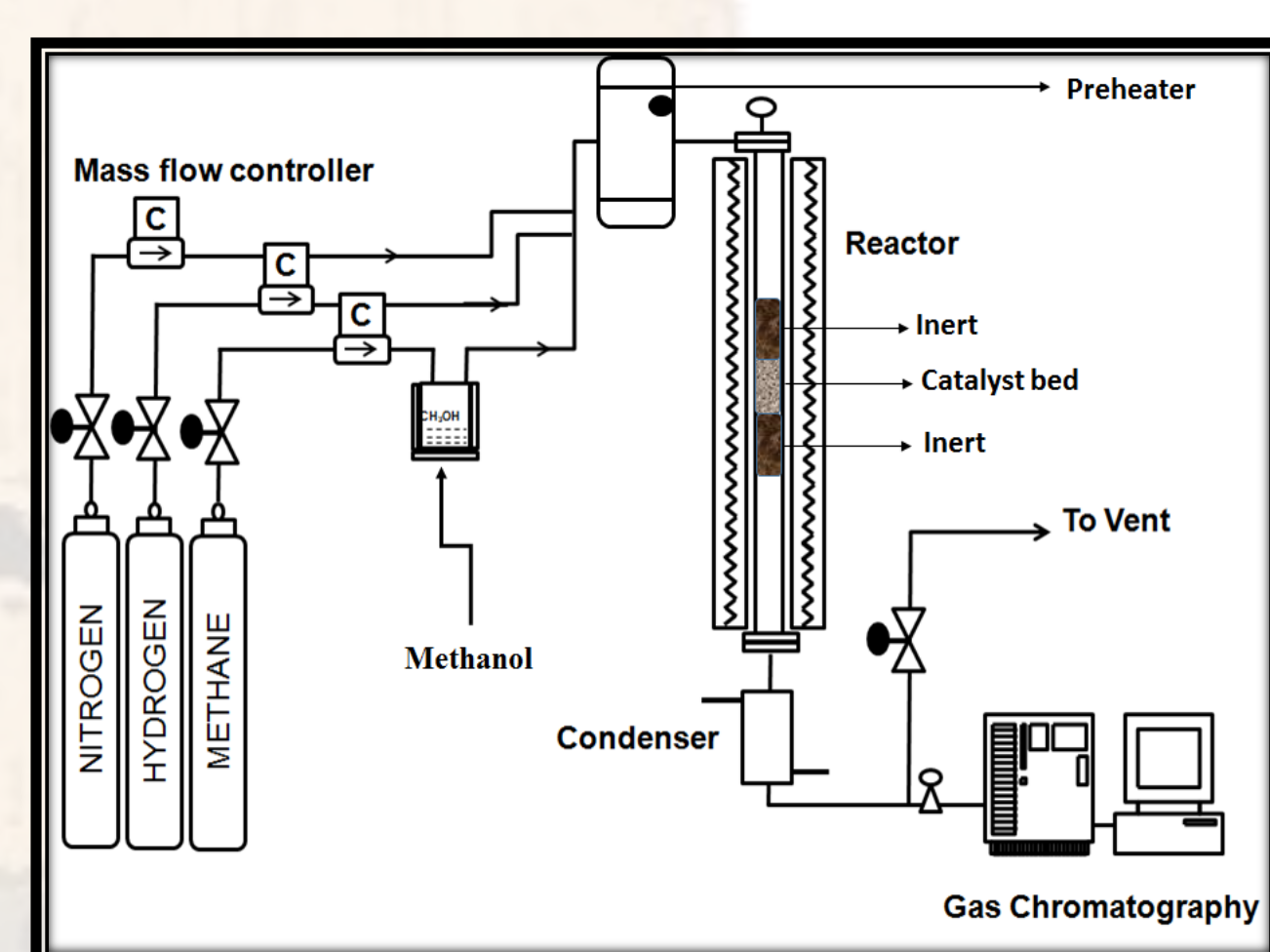
Syngas step accounts for 60% of the capital cost



Materials and Methods

- Molar gel composition for HMCM-22 zeolite: 0.30 NaOH: SiO₂: xAl₂O₃: 0.35 HMI: 45 H₂O where x (0.033, 0.025, 0.0182) varies for different SiO₂/Al₂O₃
- Mo loading over HMCM-22 support was done by conventional wet impregnation methods

Existing reactor setup



Reaction conditions

Parameters	Values
Temperature (°C)	700
Pressure	1 atm
GHSV _{CH₄} (mL/g-h)	1500

*Before activity test, catalyst was pre-treated with 25% CH₄/H₂ for carburization step

Conclusions

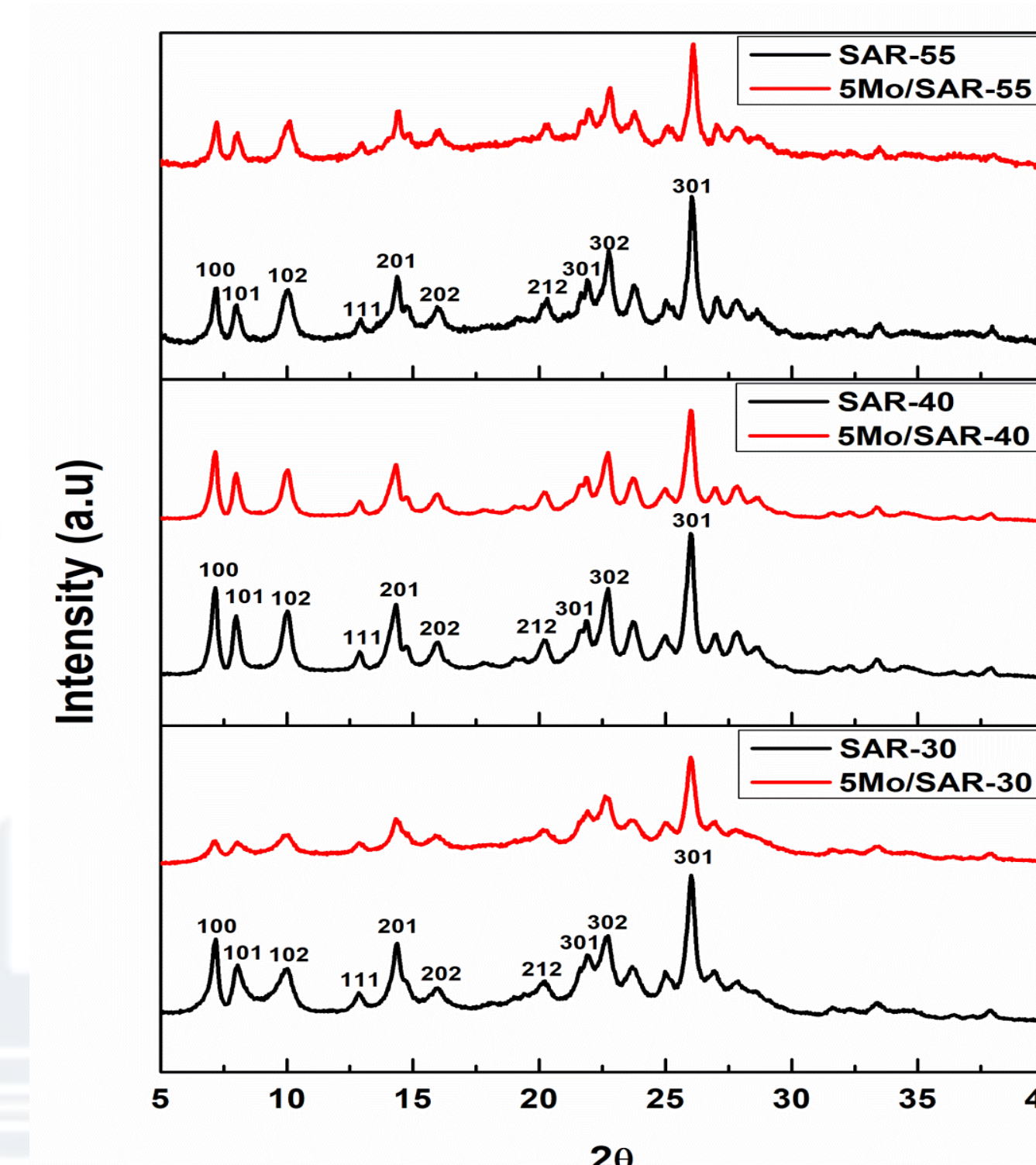
- HMCM-22 (SAR-30) with high BAS (exchangeable) concentration results high Mo dispersion
- ²⁷Al MAS NMR confirms the strong interaction with HMCM-22 having SAR-30
- 5%Mo/HMCM-22 with SAR-30 is the most active catalyst for MDA reaction in terms of high methane conversion, high benzene formation rate with lower coke deposition

Industrial Significance

- HMCM-22 zeolite is the key catalyst for aromatic alkylation and isomerization reactions
- Tuning of the framework structure significantly improves the yield of desired products
- For MDA process, which is an efficient technology for direct natural gas utilization, it results higher benzene yield (key chemical of petrochemical and polymer industries) in comparison with the conventional ZSM-5 catalyst

Results

Textural properties: XRD & BET analysis



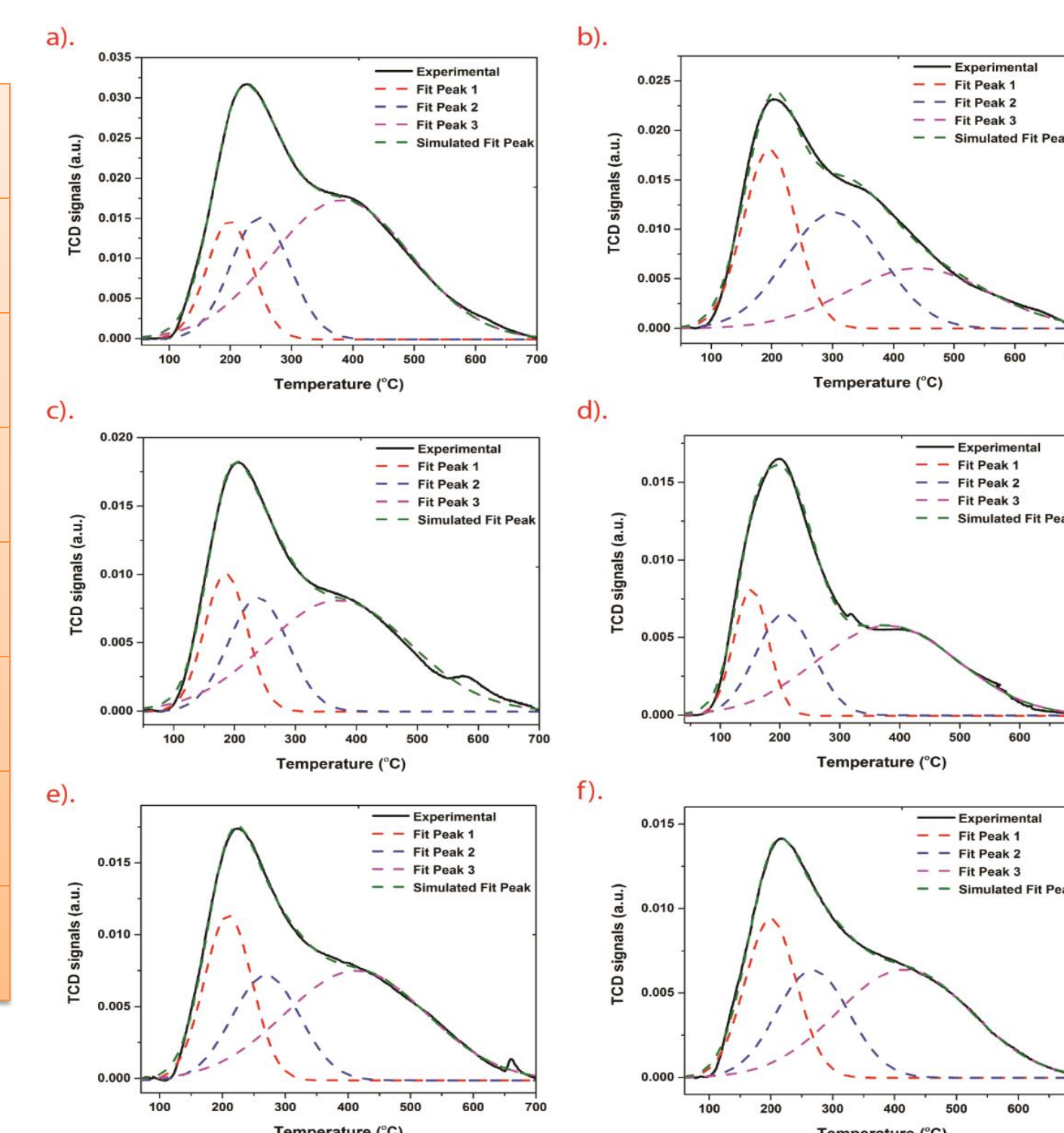
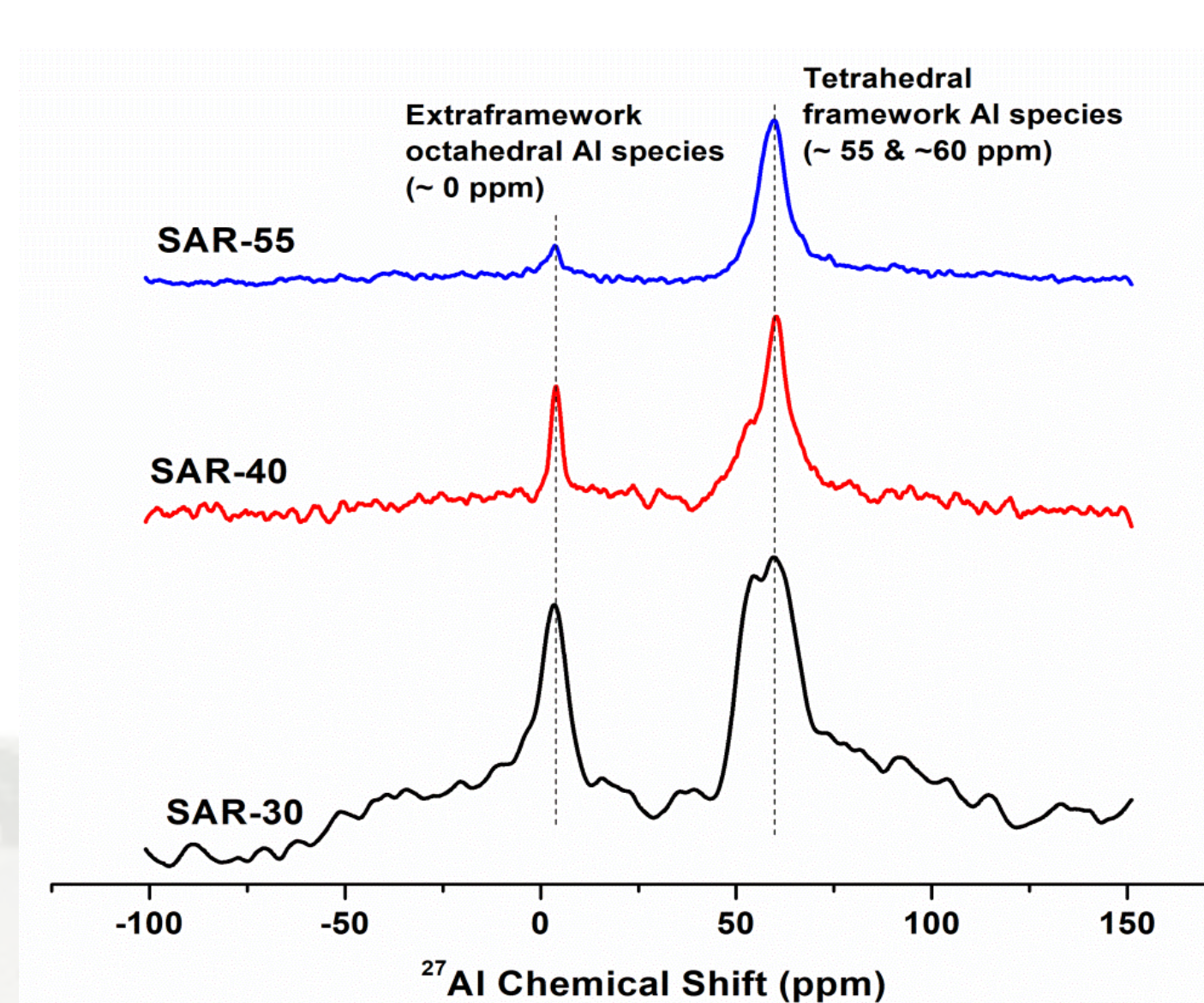
Catalyst	BET surface area (m ² /g)	Micropore Pore Volume (cm ³ /g)	Crystallinity (%)
HMCM-22 (SAR-30)	585	0.16	100
HMCM-22 (SAR-40)	458	0.13	84
HMCM-22 (SAR-55)	377	0.12	79
5Mo/HMCM-22 (SAR-30)	447	0.14	74.5
5Mo/HMCM-22 (SAR-40)	334	0.10	64.6
5Mo/HMCM-22 (SAR-55)	314	0.11	68

NH₃-TPD analysis

SAR	NH ₃ consumption, mmole/g _{cat} (Temperature, °C)			
	Peak 1	Peak 2	Peak 3	Total
30	0.29 (199)	0.38 (248)	1.02 (381)	1.69
40	0.33 (185)	0.38 (238)	0.91 (370)	1.62
55	0.35 (208)	0.32 (269)	0.69 (412)	1.36
5Mo/SAR-30	0.44 (195)	0.52 (302)	0.39 (439)	1.35
5Mo/SAR-40	0.14 (151)	0.59 (207)	0.65 (379)	1.38
5Mo/SAR-55	0.34 (199)	0.31 (268)	0.59 (415)	1.24

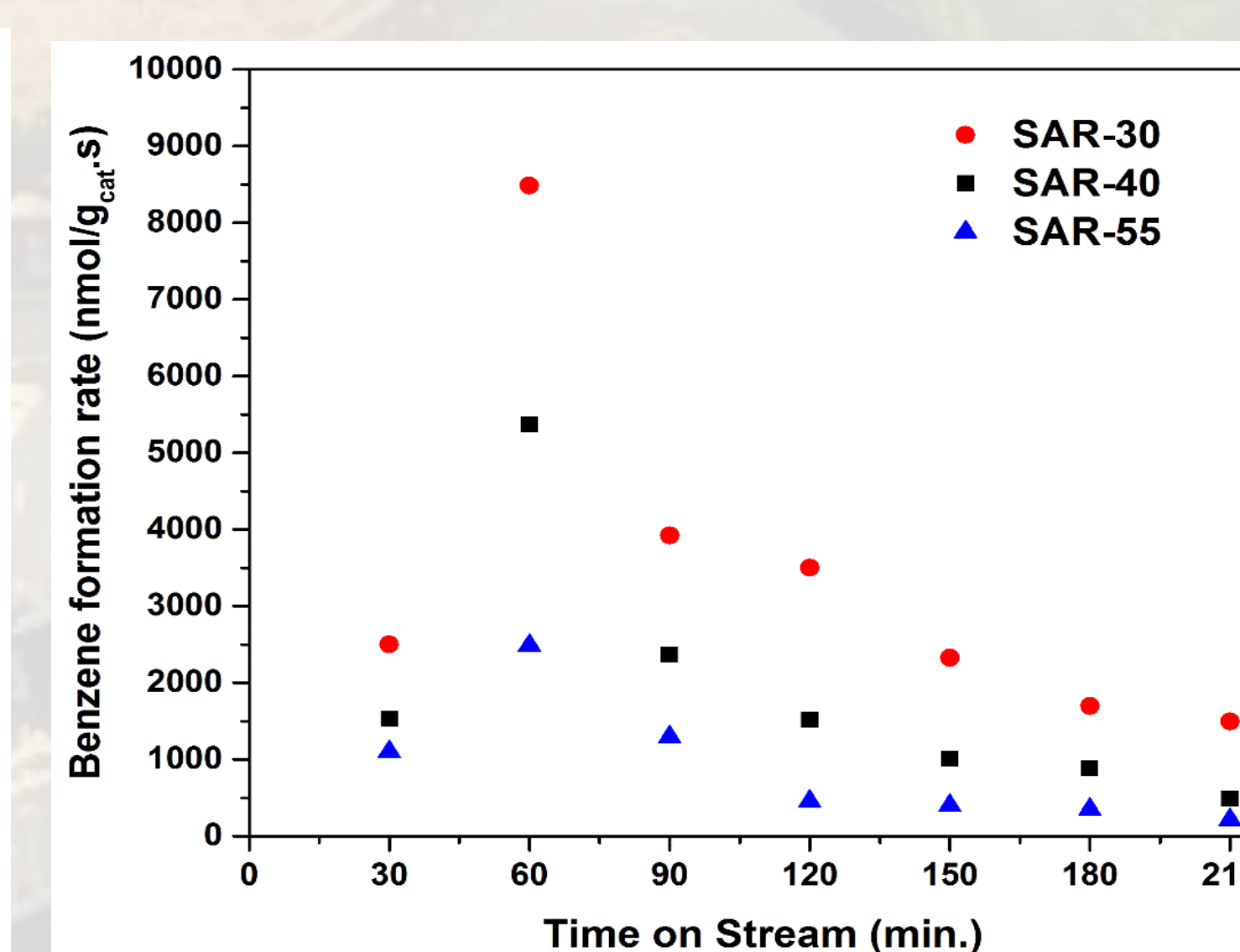
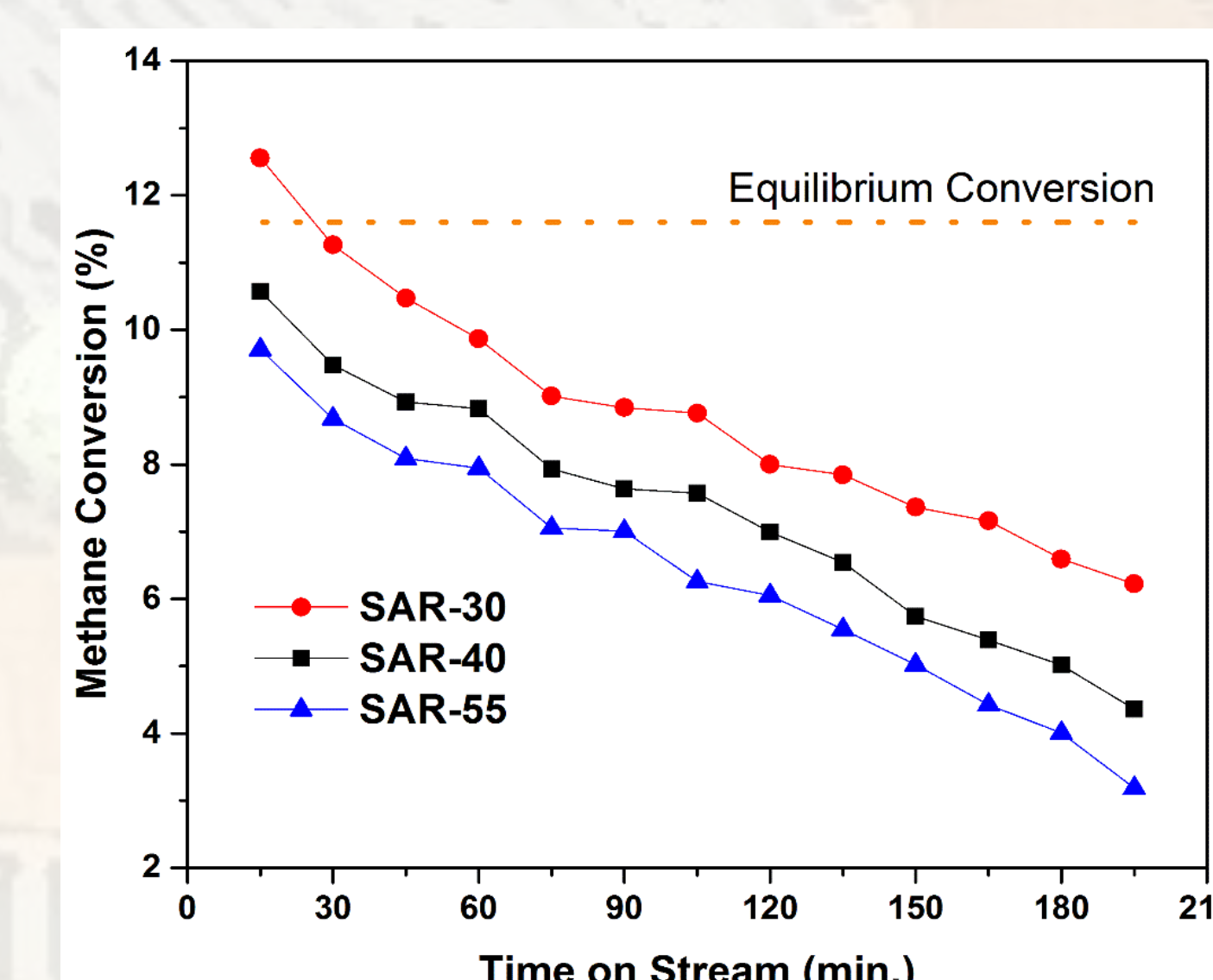
Maximum BAS (exchangeable) concentration was observed in HMCM-22 with SAR-30 resulting high Mo dispersion

²⁷Al MAS NMR analysis



(a) SAR-30 (b) 5Mo/SAR-30 (c) SAR-40 (d) 5Mo/SAR-40 (e) SAR-55 (f) 5Mo/SAR-55

Activity test



References

1. T. S. Khan, S. Balyan, S. Mishra, K. K. Pant and M. A. Haider., *J. Phys. Chem. C*, **2018**, 122 (22), 11754–11764
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